

DERIVING A TRANSPORT EQUATION FOR "φ"

φ is a "volumetric concentration" with units like kg m<sup>-3</sup> or J m<sup>-3</sup> or # m<sup>-3</sup>. ①

We want to express the idea that φ does not just appear or disappear. We introduce an imaginary "control volume" fixed in space

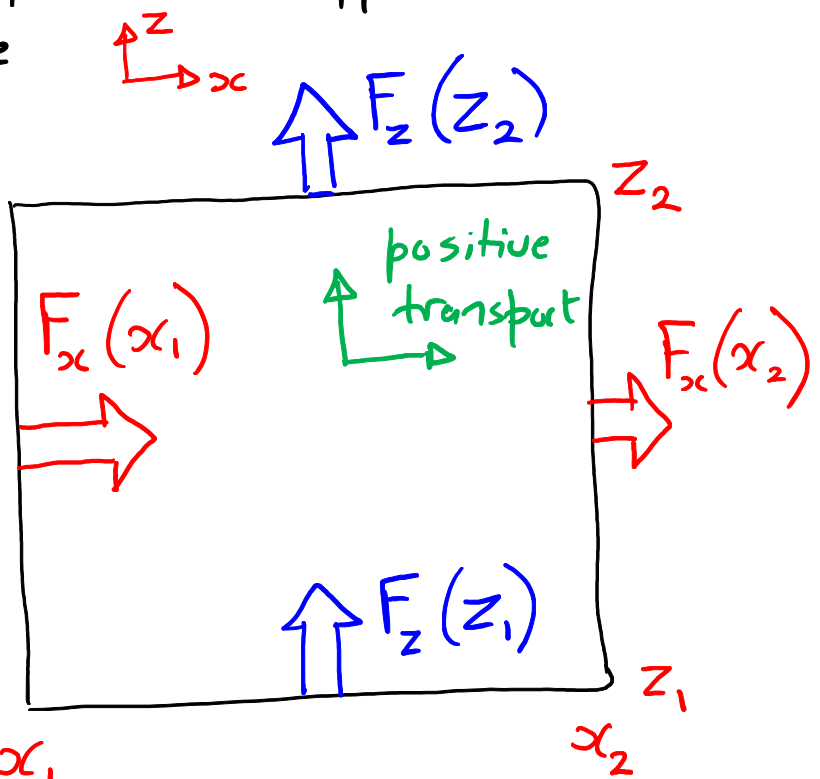
$\Delta x = x_2 - x_1, \Delta z = z_2 - z_1$

$\vec{F} = (F_x, F_y, F_z)$  the "flux density" of φ  
with units like kg m<sup>-2</sup> s<sup>-1</sup> or J m<sup>-2</sup> s<sup>-1</sup>

Consider each flux arrow to be an average along its "face".

The total amount of φ in the c.v. at time t is φ(t) Δx Δy Δz (thus φ here is implicitly the average conc. within the c.v.)

At a later time t + Δt the content of the c.v. has changed by the amount



$\Delta \phi \Delta x \Delta y \Delta z = \Delta x \Delta y \Delta z [\phi(t + \Delta t) - \phi(t)]$   
 kg or J or # = Q Δt Δx Δy Δz + net transport "T"  
 volumetric production rate, eg. kg s<sup>-1</sup> m<sup>-3</sup> (source or sink)

$$T = F_{xc}(x_1) \Delta t \Delta y \Delta z - F_{xc}(x_1 + \Delta x) \Delta t \Delta y \Delta z$$

Common to both

②

$$+ [F_z(z_1) - F_z(z_1 + \Delta z)] \Delta t \Delta x \Delta y$$

$$+ [F_y(y_1) - F_y(y_1 + \Delta y)] \Delta t \Delta x \Delta z$$

Divide through by  $\Delta t \Delta x \Delta y \Delta z$

$$\frac{\Delta \phi}{\Delta t} = Q - \frac{F_{xc}(x_1 + \Delta x) - F_{xc}(x_1)}{\Delta x} - \frac{\Delta F_y}{\Delta y} - \frac{\Delta F_z}{\Delta z}$$

where  $\Delta F_x = F_{xc}(x_1 + \Delta x) - F_{xc}(x_1)$

Finally, take limit  $\Delta t, \Delta x, \Delta y, \Delta z \rightarrow 0$

$$\frac{\partial \phi}{\partial t} = - \frac{\partial F_{xc}}{\partial x} - \frac{\partial F_y}{\partial y} - \frac{\partial F_z}{\partial z} + Q = - \nabla \cdot \vec{F} + Q$$

local  
tendency

(these are all partial derivatives)

transport      production

Transport mechanisms? Mass Energy

③

① convection ("bulk flow")  $\vec{F}_{\text{conv}} = \vec{u} \phi$

② diffusion "Fick's Law"  $\vec{F}_{\text{diff}} = -D \nabla \phi$   $\left[ \frac{\text{m}^2}{\text{s}} \quad \frac{1}{\text{m}} \quad \frac{\text{kg}}{\text{m}^3} \right] \checkmark$

$\uparrow$   
molecular diffusivity  $\text{m}^2 \text{s}^{-1}$

① convection  $\vec{u} \phi$

② conduction  $-D \nabla \phi$

③ radiation  $\vec{R}$

In the atmos., convection is by far more important than diffusion/conduction

\*  $\vec{F}_{\text{diff}} = -D \left( \frac{\partial \phi}{\partial x}, \frac{\partial \phi}{\partial y}, \frac{\partial \phi}{\partial z} \right)$

Fourier's Law of Heat Conduction

$\vec{F} \left[ \frac{\text{W}}{\text{J s}^{-1} \text{m}^{-2}} \right] = -k \nabla T$

conductivity  $\text{W m}^{-1} \text{K}^{-1}$

Recall that "convective transport" is not necessarily "driven" by buoyancy and not necessarily oriented along the vertical